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## PENETRATIVE CONVECTIVE INSTABILITIES IN PARALLEL FLOWS

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## ABSTRACT

An analysis has been performed of penetrative convective instabilities arising from the combined action of thermal and centrifugal buoyancy forces. The theory allows for the fact that in the atmosphere, convection arising in an unstable layer may penetrate into a neighboring stable region. The objective has been to examine the effect of various mean temperature and velocity profiles on the critical limit and convective penetration of the disturbances. The linearized perturbation equations have been solved employing an approximate technique. The results obtained indicate that nonlinear profiles are more unstable and penetrative than linear ones. The close analogy between streamline curvature and thermal stratification effects has been demonstrated. It is found that for parallel layers of fluid along curved heated walls, a unique stability curve for neutral disturbances may be obtained if the quantity plotted along the abscissa is Ra +  $\kappa N_G^2$  where Ra is the Rayleigh Number, N<sub>G</sub> is the Goertler Number and  $\kappa$  a constant which expresses the relative importance of the mean temperature and velocity profiles.

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# LIST OF SYMBOLS

Symbol	Definition
ũ	Horizontal velocity perturbation
v	Vertical velocity perturbation
Ŵ	Lateral velocity perturbation
~ p	Pressure perturbation
$\tilde{\mathbf{T}}$	Temperature perturbation
U	Mean flow (undisturbed) horizontal velocity
Т	Mean temperature
k	Curvature
Pr	Prandtl Number
N <sub>G</sub>	Goertler Number
Ra	Rayleigh Number
x,y,z	Streamwise, vertical and lateral directions, respectively
R <sub>δ</sub>	Reynold's Number $(=\frac{U_{\infty\delta}}{v})$
с	Penetration coefficient
d	Total depth of penetration
g	Gravitational acceleration
t	Time
f	Dimensionless velocity profile T - T
T*	Dimensionless temperature (= $\frac{1}{T_{w}} - \frac{1}{T_{w}}$ )
Δ <b>T</b>	Temperature difference across unstable layer
β	Volumetric expansion coefficient
ν	Kinematic viscosity
Х	Stability parameter
Φ	Dimensionless wavenumber

## LIST OF SYMBOLS - (Continued)

# $\begin{array}{c} \underline{Symbol} & \underline{Definition} \\ \delta & Characteristic thickness of boundary layer \\ \xi & Transformed vertical coordinate \\ \alpha & Wavenumber \end{array}$

# Subscript

- p y dependent part of perturbations
- w Conditions at wall (y = 0)
- $\infty$  Conditions at edge of unstable layer (y =  $\delta$ )

#### PENETRATIVE CONVECTIVE INSTABILITIES IN PARALLEL FLOWS

#### I. INTRODUCTION

This discourse considers penetrative convective instabilities resulting from the combined action of thermal and centrifugal buoyancy forces. These instabilities are assumed to take the form of steady three dimensional vortices oriented in the streamwise direction and are similar to the disturbances observed in the flow between rotating concentric cylinders. The latter instability manifests itself in the form of regularly spaced toroidal vortices stacked around the inner cylinder. This phenomenon was first examined by Taylor (1) who formulated the motion in mathematical terms, analyzed its stability and verified the analysis in quite conclusive fashion. If the inner cylinder is sufficiently far removed that the flowfield reduces to that of a boundary layer along a curved wall, the instabilities induce a secondary flow of parallel streamwise oriented vortices. Goertler (2) and later Smith (3) investigated the vortex mode of motion along a plate with concave curvature and indicated the presence of a system of parallel counter rotating vortices aligned in the mean flow direction. Furthermore, their analyses clearly indicated that only flows with concave curvature were susceptible to this type of instability. Experimental verification was subsequently obtained by Goertler (2), Liepmann (4) and Tani (5). The parameter governing the stability of the flow is the Goertler Number  $R_{g}\sqrt{k\delta}$  where  $R_{g}$  is the Reynolds Number based on the boundary layer thickness,  $\delta$  , and k is the curvature of the wall.

The analogy between flows with concave curvature and buoyancy due to unstable stratification was pointed out by Goertler (6) and more recently by Yih (7) and by Bradshaw (8). Terada (9) and Sparrow  $\underline{\text{et al.}}$  (10), have observed the vortex mode of motion in the flows of liquids down inclined heated plates.

The occurrence of a closely analogous phenomenon in the atmosphere is fairly well documented. The large-scale cloud streets frequently observed in satellite photographs are now accepted as direct evidence of the presence of longitudinal vortex instabilities in the earth's atmosphere. The clouds are formed as a result of the convective action of the rolls in lifting moist air to its condensation level. Further direct evidence is supplied by the experience of glider pilots (11), who have made use of these 'invisible highways' in the air to soar over large distances. Kuo (12) analyzed the stability of plane Couette flow with a suitable gradient of potential temperature so as to model the atmospheric boundary layer. However, his boundary conditions required the physically unrealistic situation of a rigid upper bounding surface.

The present study allows for the fact, that in the atmosphere, convection arising in an unstable layer may penetrate into a neighboring stable region. This in fact, was implied in a paper by Kuettner (11) who observed that cloud streets frequently had well defined tops indicating the presence of an elevated inversion. An additional consideration is that when there is a mean shear, the role of penetrative convection in vertical transfer of heat, moisture, and momentum may be important, as indicated in a recent paper by Estoque (13). The penetrative action of the instabilities into the stable region may be due to two causes, viz., a) the nonvanishing of the vertical velocity components of the disturbances at the interface causing inertial penetration or b) momentum being transferred into the upper

layer by viscous interaction of the perturbations with the adjoining stable fluid. The outer system of vortices observed in Taylor's experiment was due to this second type of penetration.

Inertial penetration has been studied extensively (see, for example, Stix (14), and Whitehead and Chen (15)), while penetration by viscous entrainment has been studied recently by Rintel (16). The analysis described herein, assumes that the penetration is of the second type and follows closely the work of Rintel. In this approximation, the instabilities generated in a layer of fluid of thickness  $\delta$ , penetrate to a total height d into neighboring stable fluid. A quantity  $c = \frac{d}{\delta}$  called the penetration coefficient provides an estimate of the degree of penetration.

Solutions have been obtained for a variety of flows along heated curved walls with stable\* fluid overhead. In most cases, the raison d'etre has been to model atmospheric type<sup>†</sup> instabilities and to demonstrate more clearly the analogy existing between flows with concave curvature and unstable stratification. Consequently, the Tollmein-Schlichting wave-type disturbances pertinent to transtion are not accounted for in this analysis. However, for heated or curved flowfields the Squire theorem does not necessarily hold (17); hence three dimensional disturbances may be the more unstable mode. Furthermore, these stationary convective motions have been observed to persist in turbulent fluid by Tani (5) where the problem of transition does not arise. The specific cases of the parallel flows whose stability

<sup>\*</sup>In this context 'stable' refers to stability with respect to velocity gradient, i.e., where Rayleigh's inviscid stability criterion is satisfied as well as the conventional interpretation of stable temperature stratification.

<sup>&</sup>lt;sup>†</sup>It is realized of course, that the atmospheric situation is complex, with anistropic turbulent diffusivities of heat and momentum. Nevertheless, some qualitative results may be inferred.

are examined herein are:

- a) Heated flat plate boundary layer
- b) Parallel flow with free surface along curved heated walls
- c) Boundary layer type flow with wall curvature and heating bounded above by fluid with differing stable gradients of temperature and velocity
- d) Stationary layer of fluid with strongly non-linear temperature distribution bounded by mildly stable fluid
- e) Stationary layer of fluid with parabolic mean temperature profile posed as a problem in penetrative convection

Details of the cases examined will be discussed later.

#### II. Theoretical Development

Consider an unstably stratified parallel flow over a curved surface. The unstable layer is considered to be bounded above by fluid of neutral or arbitrarily specified stability. It is assumed that the disturbances generated in the lower layer of thickness  $\delta$  penetrate to a height d. The penetration coefficient is then defined as  $c = \frac{d}{\delta}$ . The parameter c thus provides a measure of the extent of penetration. In this respect it is closely allied to the "effective depth" defined by Kuo (12).

We start with the Navier-Stokes equations of motion and the energy equation, expressed in a curvilinear coordinate system (Fig. (1)). Using the Boussinesq approximation, one can derive the following equations for the perturbations  $\tilde{p}$ ,  $\tilde{T}$ ,  $\tilde{u}_i$  of pressure, temperature and the three components of velocity, respectively.

$$\frac{\partial \tilde{u}}{\partial t} + \tilde{v} \frac{\partial U}{\partial y} + k\tilde{v}U + \tilde{w} \frac{\partial U}{\partial z} = v \left\{ \frac{\partial^2 \tilde{u}}{\partial y^2} + \frac{\partial^2 \tilde{u}}{\partial z^2} + k \frac{\partial \tilde{u}}{\partial y} \right\}$$

$$\frac{\partial \tilde{v}}{\partial t} - 2k\tilde{u}U = g\beta\tilde{T} - \frac{1}{\rho} \frac{\partial \tilde{p}}{\partial y} + v \left\{ \frac{\partial^2 \tilde{v}}{\partial y^2} + \frac{\partial^2 \tilde{v}}{\partial z^2} + k \frac{\partial \tilde{v}}{\partial y} \right\}$$
(1)
$$\frac{\partial \tilde{w}}{\partial t} = -\frac{1}{\rho} \frac{\partial \tilde{p}}{\partial z} + v \left\{ \frac{\partial^2 \tilde{w}}{\partial y^2} + \frac{\partial^2 \tilde{w}}{\partial z^2} + k \frac{\partial \tilde{w}}{\partial y} \right\}$$

$$\frac{\partial \tilde{v}}{\partial y} + \frac{\partial \tilde{w}}{\partial z} + k\tilde{v} = 0$$
(2)
$$\frac{\partial \tilde{T}}{\partial t} + \tilde{v} \frac{\partial T}{\partial y} + \tilde{w} \frac{\partial T}{\partial z} = \frac{v}{P_r} \left\{ \frac{\partial^2 \tilde{T}}{\partial y^2} + \frac{\partial^2 \tilde{T}}{\partial z^2} + k \frac{\partial \tilde{T}}{\partial y} \right\}$$
(3)

where k denotes the curvature, v, the kinematic viscosity,  $\beta$ , the volume expansion coefficient and g the gravitational acceleration. One can analyze an arbitrary disturbance into a set of normal modes

$$\tilde{u} = u_{p}(y) \quad \cos \alpha z \quad e^{\beta_{1}t}$$

$$\tilde{v} = v_{p}(y) \quad \cos \alpha z \quad e^{\beta_{1}t}$$

$$\tilde{w} = w_{p}(y) \quad \sin \alpha z \quad e^{\beta_{1}t}$$

$$\tilde{T} = T_{p}(y) \quad \cos \alpha z \quad e^{\beta_{1}t}$$

$$\tilde{p} = p_{p}(y) \quad \cos \alpha z \quad e^{\beta_{1}t}$$

and since we consider only neutral disturbances we substitute the above disturbances into equations (1) to (3) with  $\beta_1 = 0$ . The justification for this step lies in the validity of the principle of the "exchange of stabilities" for such flows (15,18). This results in the following system of differential equations:

$$\mathbf{v}_{\mathbf{p}}\left(\frac{\partial U}{\partial \mathbf{y}} + \mathbf{k}U\right) = -\nu\{\mathbf{u}_{\mathbf{p}}^{\prime\prime} + \mathbf{k}\mathbf{u}_{\mathbf{p}}^{\prime} - \alpha^{2}\mathbf{u}_{\mathbf{p}}\}$$
(4)

$$2kUu_{p} = g\beta T_{p} - \frac{p_{p}'}{\rho} + \nu \{v_{p}'' + kv_{p}' - \alpha^{2}v_{p}\}$$
(5)

$$0 = \alpha \frac{p_{p}}{\rho} + \nu \{w_{p}'' + kw_{p}' - \alpha^{2}w_{p}\}$$
(6)

$$0 = v'_p + kv_p + \alpha w_p$$
<sup>(7)</sup>

$$\mathbf{v}_{\mathbf{p}} \frac{\partial \mathbf{T}}{\partial \mathbf{y}} = \frac{\mathbf{v}}{\mathbf{p}} \{\mathbf{T}_{\mathbf{p}}^{"} + \mathbf{k}_{\mathbf{p}}^{T} - \alpha^{2} \mathbf{T}_{\mathbf{p}}\}$$
(8)

 $\boldsymbol{\alpha}$  is of course the horizontal wavenumber of the perturbations.

For solution of these equations, the 'rigid-free' boundary conditions (Chandrasekhar (18)) are assumed. That is, the plane y = 0 is taken to be a rigid surface with  $y = \delta$  being a free surface. The boundary conditions are then

$$v_p = (D^2 - \alpha^2)^2 v_p = 0$$
 for  $y = 0$  and  $\delta$   
 $v_p' = 0$  at  $y = 0$  and  $v_p'' = 0$  at  $y = \delta$ 

By eliminating  $p_p$  and  $w_p$  and discarding higher order curvature terms, equations (4) to (8) may be reduced to

$$(D^{2} - \alpha^{2})^{2} v_{p} = \frac{\alpha^{2}}{\nu} (g\beta T_{p} - 2kUu_{p})$$
(9)

$$(D^{2} - \alpha^{2}) u_{p} = \frac{-v_{p}}{v} \left(\frac{\partial U}{\partial y} + kU\right)$$
(10)

$$(D^{2} - \alpha^{2}) T_{p} = \frac{Pr}{v} \frac{\partial T}{\partial y} v_{p}$$
(11)

Here  $D \equiv \frac{d}{dy}$  and U and T refer to the undisturbed mean velocity and temperature respectively.

Defining dimensionless quantities  $\phi = \alpha \delta$ ,  $\bigoplus' = \frac{g\beta\delta^2}{\nu}$ ,  $\gamma' = \frac{2kU_{\infty}\delta^2}{\nu}$ ,  $R_{\delta} = \frac{U_{\infty}\delta}{\nu}$ ,  $f = \frac{U}{U_{\infty}}$ ,  $f' = \frac{\partial f}{\partial y}$ ,  $T'_* = \frac{\partial T}{\partial y} \frac{1}{\Delta T}$  with y made dimensionless with respect to  $\delta$  and  $\Delta T$  the temperature difference across the fluid layer, equations (9), (10), and (11) become

$$(D^{2} - \phi^{2})^{2} v_{p} = \phi^{2} ( \bigoplus ' T_{p} - fu_{p} \gamma')$$
(9a)

$$(D^{2} - \phi^{2}) u_{p} = -(v_{p}R_{\delta}f' + v_{p}R_{\delta}fk\delta)$$
(10a)

$$(D^{2} - \phi^{2}) T_{p} = \delta \frac{Pr}{v} \Delta T T_{\star}^{*} v_{p}$$
(11a)

As stated earlier, the penetration coefficient c is defined as the ratio of the penetrated height d to the thickness  $\delta$  of the unstable layer. We therefore define a new dimensionless coordinate  $\xi = \frac{y}{c}$  and the modified parameters  $(H) = c^2(H)'$ ,  $\Phi = c\phi$ ,  $\gamma = c^2\gamma'$ and a modified Reynolds Number  $R_{c\delta} = cR_{\delta}$ . Eliminating the second term on the right hand side of equation (10a) since the product  $k\delta$ is always small, one obtains with the above dimensionless parameters the final form of the differential equations for the perturbations viz.,

$$(D^{2} - \Phi^{2})^{2} \mathbf{v}_{p} = \Phi^{2}((\widehat{\mathbf{H}} \mathbf{T}_{p} - \mathbf{f}(c\xi)\mathbf{u}_{p}\delta)$$
(12)

$$(D^{2} - \Phi^{2}) u_{p} = -v_{p} R_{c\delta} f'(c\xi)$$
(13)

$$(D^{2} - \phi^{2}) T_{p} = v_{p} Pr \frac{c\delta}{v} \Delta T T'(c\xi)$$
(14)

where  $D \equiv \frac{d}{d\xi}$ . The revised boundary conditions are

$$T_{p} = u_{p} = 0 \text{ for } \xi = 0 \text{ and } 1$$
$$v_{p} = Dv_{p} = 0 \text{ for } \xi = 0$$
$$v_{p} = D^{2}v_{p} = 0 \text{ for } \xi = 1$$

Equations (12) to (14) are solved approximately using a technique devised by Chandrasekhar (18). The parallel and normal to the wall components of the perturbation velocity are expanded in a series of functions satisfying the boundary conditions for a rigid wall at  $\xi = 0$  and a free surface boundary at  $\xi = 1$ .

$$u_{p} = \sum_{n=1}^{\infty} B_{n} x_{n}$$

$$v_{p} = \sum_{n=1}^{\infty} A_{n} z_{n}$$
(15)

The temperature perturbation, since it satisfies similar boundary conditions as  $u_p$  is written as

$$T_{p} = \sum_{n=1}^{\infty} C_{n} x_{n}$$
(15)

where we choose

$$\lambda_{n}^{2} x_{n} = \sin n\pi\xi$$

$$\lambda_{n}^{2} z_{n} = \lambda_{n}^{2} x_{n} + \frac{2n\pi}{\sinh 2\Phi - 2\Phi} \{\sinh\Phi\xi - \xi\sinh\Phi\cosh(\Phi\xi - \Phi)\}$$

$$\lambda_{n}^{2} = n^{2}\pi^{2} + \Phi^{2}$$

It may be readily verified that the functions chosen satisfy the boundary conditions and also that

$$(D^{2} - \Phi^{2}) x_{n} = -\lambda_{n} x_{n}$$
$$(D^{2} - \Phi^{2}) z_{n} = \lambda_{n} z_{n}$$

When these expressions are substituted into the differential equations and the coefficients  $B_n$  and  $C_n$  are eliminated, the following eigenvalue system is obtained for  $A_n$ .

$$A_{n} = c^{3} \phi^{2} \{ 8N_{G}^{2} \sum_{m=1}^{\infty} \frac{X_{nm}^{\prime}}{\lambda_{m}} \sum_{\ell=1}^{\infty} \frac{A_{\ell} Y_{\ell n}^{\prime}}{\lambda_{\ell}} + 2Ra \frac{1}{\lambda_{n}} \sum_{m=1}^{\infty} \frac{A_{m}}{\lambda_{m}} Y_{mn}^{0} \}$$
  
where  $N_{G} = R_{\delta} \sqrt{k\delta}$  is the Goertler Number and  $Ra = \frac{g\beta\delta^{3}\Delta T}{\nu K}$  is the Rayleigh Number with

$$\begin{aligned} \mathbf{x}_{nm}^{\prime} &= \lambda_{n} \lambda_{m} \int_{0}^{1} \mathbf{f} \mathbf{x}_{m} \mathbf{x}_{n} d\xi \\ \mathbf{y}_{\ell n}^{\prime} &= \lambda_{\ell} \lambda_{n} \int_{0}^{1} \mathbf{f}^{\prime} \mathbf{z}_{\ell} \mathbf{x}_{n} d\xi \\ \mathbf{y}_{mn}^{0} &= \lambda_{m} \lambda_{n} \int_{0}^{1} \mathbf{T}^{\prime} \mathbf{z}_{m} \mathbf{x}_{n} d\xi \end{aligned}$$

The standard method of evaluating the Fourier coefficient has been used to arrive at the previous equation. It may now be rewritten as

$$A_{n} = c^{3} \phi^{2} \sum_{\ell=1}^{\infty} A_{\ell} \{ 8N_{G}^{2}P_{\ell n} + 2RaQ_{\ell n} \} = c^{3} \phi^{2} \sum_{\ell=1}^{\infty} A_{\ell}R_{\ell n}$$
(16)

Here  $Q_{\ell_n} = \frac{Y_{\ell_n}^o}{\lambda_{\ell}\lambda_n}$ ,  $P_{\ell_n} = \sum_{m=1}^{\infty} \frac{X'_{nm}Y'_{\ell_m}}{\lambda_{\ell}\lambda_m}$ 

In matrix notation we have the familiar eigenvalue problem

$$[A] = \Phi^2 c^3 [R] [A]$$

The equation of neutral stability is then

$$\left|\delta_{nm} - c^{3} \phi^{2} R_{nm}\right| = 0$$

To simplify numerical evaluation of equation (16), it is rewritten in the form

$$A_{n} = c^{3} \phi^{2} N_{G}^{2} \sum_{\ell=1}^{\infty} A_{\ell} \{ 8P_{\ell n} + 2R_{n}Q_{\ell n} \}$$
(17)

where  $R_N$  is defined as  $\frac{Ra}{N_G^2}$ . It therefore expresses the relative importance of buoyancy forces to centrifugal inertial forces with viscous damping as an overall effect. Equation (17) was solved for various values of the  $R_N$  number.

#### III. Outline of Solution Procedure

Numerical evaluation of the eigenvalue problem was performed on a CDC 6400 computer. The method consisted in minimizing the Goertler or Rayleigh Number as a function of the wavenumber  $\Phi$  and penetration coefficient c. The method is well described by Rintel (16). A complete neutral stability curve may be generated by varying  $\Phi$ keeping c at its critical value. The results thus obtained are scaled with the critical c value. A more accurate representation would be obtained if c is minimized at each point on the stability curve. This, however, ceases to be economical in terms of computer time. For cases of combined heating with wall curvature, equation (17) was used with  $R_n$  being treated as a parameter. For purposes of numerical evaluation, the infinite series expansion in equation (15) was truncated to thirty terms and the matrices were limited to fifth order. For the cases where penetration was into neutrally stable fluid, the order of the matrices used was increased to nine. A check, performed by increasing the truncation order of both the series and the matrices, revealed that this provided sufficient accuracy.

The mean flow profiles for the cases examined are listed below.

(a) The heated flat plate boundary layer

$$f(y) = 2y - 2y^3 + y^4 \quad 0 \le \xi \le \frac{1}{c}$$

matched at  $\xi = \frac{1}{c}$  with

$$f(y) = \chi(2y - 2y^3 + y^4) + 1 - \chi \quad \frac{1}{c} \le \xi \le 1$$

where  $y = c\xi$  and  $\chi$  is a parameter used to represent the stability of the outer "freestream" gradient.  $\chi$  was set equal to  $10^{-8}$  in this case, to represent a neutrally stable freestream. The Prandtl Number was taken as unity. Critical conditions were evaluated with two

types of mean thermal profile, the first being identical to the Pohlhausen profile above and the second, a linear one:

- $T_*(y) = y$   $o \leq \xi \leq \frac{1}{c}$
- $T_{\star}(y) = -\chi y \qquad \frac{1}{c} \leq \xi \leq 1$

with  $\chi = 10^{-8}$ . Here  $T_* = \frac{T - T_w}{T_{\infty} - T_w}$  where  $T_{\infty}$  = temperature at edge of unstable layer,  $T_w$  = wall temperature.

(b) Parallel flow with free surface along curved heated wall

$$f(y) = y(2 - y)$$
  
 $\Gamma_{+}(y) = y$ 

were assumed for the mean velocity and temperature profiles respectively with unit Prandtl Number. Since the fluid layer was assumed to have a free surface, the penetration was taken as zero implying c = 1.

(c) Boundary layer type flow with combined wall curvature and heating

$$f(y) = y(2-y) \qquad 0 \le \xi \le \frac{1}{c}$$
  
$$f(y) = xy(2-y) + 1 - \chi \qquad \frac{1}{c} \le \xi \le 1$$

The same mean temperature profile was assumed except that x was taken as one for the velocity profile and three for the temperature profile. This served to demonstrate the generality of the method while also approximating a possibly real situation in the atmosphere. A value of 0.7 for the Prandtl Number was used in evaluating this case. A semiempirical adjustment for this was made in evaluating the integral  $Y_{mn}^{o}$  by defining a new variable  $\xi_1 = \xi \operatorname{Pr}^{1/3}$  according to Eckert and Drake (19). Hence, when the integration of  $\xi$  is carried over the range 0 to 1, the entire thermal profile is integrated across simultaneously.

(d) Stationary layer of fluid with strongly non-linear temperature profile

$$T_* = y - N_s y(y-1) \qquad 0 \le \xi \le \frac{1}{c}$$
$$T_* = -\chi y \qquad \qquad \frac{1}{c} \le \xi \le 1$$

with  $\chi$  = 0.5 and  $N_{\rm s}$  = 40 .

This profile is one proposed by Sparrow, Goldstein and Jonsson (20) as being indicative of internally distributed heat sources. However, Such a profile is not uncommon in the lower layers of the atmosphere, where the release of latent heat would generate non-linear temperature distributions. As stated above, the unstable layer is capped by fluid of moderate stability. The results to be presented later indicate strongly penetrative convection.

(e) Stationary layer of fluid with parabolic thermal profile posed as a problem in penetrative convection in this example:

$$T_{*} = y(2-y) \qquad \qquad 0 \le \xi \le \frac{1}{c}$$
$$T_{*} = \frac{1}{(c-1)^{2}} [y(2-y) - c(2-c)] \qquad \frac{1}{c} \le \xi \le 1$$

#### IV. Discussion of Results

The cases for which the critical conditions were evaluated have been listed earlier, however, in order to facilitate easy comparison they are listed in Table 1 together with the corresponding results.

		Mean Velocity	Mean Temperature	C <sub>cr</sub>	${}^{\Phi}$ cr	<sup>Ra</sup> cr	<sup>N</sup> Gcr
Case	(a)	Profile Pohlhausen	Profile Pohlhausen Linear	2.2325 2.0263	2.9265 2.7119	735.9 311.1	
Case	(b)	Parabolic	Linear	1.0	2.656		
Case	(c)	See Table II					
Case	(d)		Nonlinear	2.1362	2.9447	15.217	/3
Case	(e)		Parabolic	1.2325	2.71	997.8	

TABLE 1

The first case examined, viz., the boundary layer on a heated flat plate is relevant to the transition mechanism due to thermal stratification effects. An examination of the dimensionless disturbance velocity components in Fig. (2) provide a measure of the degree of penetration of the longitudinal vortices into the freestream. This penetrative action of the vortices has been experimentally observed by Sparrow and Husar (10). The critical Rayleigh numbers have been calculated to be approximately 736 for the Pohlhausen profile and 311 for the linear profile and are listed for convenience in Table II. The point of first instability is therefore highly dependent on the shape of the profile in the unstable layer. Since the system of equations (4) to (8) are coupled in only a linear manner, the onset of convective instability is independent of the shear, a result that is also stated by Gage and Reid (17). (The effect of the shear is only to cause the appearance of the longitudinal rolls without which

stationary Benard type convection occurs). The Pohlhausen temperature profile causes stronger penetration than the linear one, although the latter profile is more unstable.

The penetrative character of the disturbances causes a marked reduction in the critical Rayleigh Number. This may be appreciated by comparing the classical non-penetrative result of Ra = 1100 with the result obtained here of 311.1. This value of the critical Rayleigh Number obtained does not agree with those of Rintel (12). A closer examination of his work indicated that he had drawn an incorrect analogy between the narrow gap Taylor problem and the Bénard problem. Such an analogy follows only when the mean temperature profile is linear and continuous throughout the inner and outer (stable) region. Since in fact, the values in his Table II (12) were arrived at by integrating over a region with a discontinuity in the mean thermal profile they are incorrect <sup>ex</sup>cept for the limiting case with c = 1 and  $\chi = \infty$  since then the discontinuity ceases to exist.

It should be noted that the eigenfunctions for the temperature and horizontal velocity perturbations are identical when the mean thermal and velocity profiles are the same with Prandtl Number equal one, but different otherwise.

Figure (3) illustrates the results obtained for case (b), i.e., the stability of a parallel free surface flow along a curved heated wall with zero penetration. The analogy between curvature and buoyancy is well displayed in Fig. (4) which is a composite neutral stability curve obtained by plotting  $\Phi$ , the disturbance wavenumber versus  $N_{\rm G}^2 + \kappa Ra$ . This result was arrived at as follows: A previous simple analyses by the authors, of curved flows with thermal stratification,

had yielded the parameter  $N_G^2$  + Ra as a stability criterion for linear profiles. It was, therefore, intuitively expected that nonlinear profiles would perhaps yield the slightly more general parameter  $N_G^2$  +  $\kappa$ Ra where  $\kappa$  now, would account for the differences between the thermal and velocity profiles. Consequently, a number of calculations of the stability boundaries for various values of the parameter  $R_n$  were performed. It was then easy to calculate  $\kappa$  and establish that  $N_G^2$  +  $\kappa$ Ra was indeed a unique parameter by checking several points on the calculated curves.

A secondary dependence of  $\kappa$  would be on the degree of penetration into the stable fluid, a limiting factor in establishing this dependence being the computer time available. To examine this effect, a small number of calculations were run on case (c) and the critical values obtained in a first approximation in the minimization are given in Table II.

N <sub>G</sub> cr	Rn	Ra	<sup>Φ</sup> cr	C <sub>cr</sub>	к	
21.76	0	0.0	2.6943	1.4512	<b>~ ~</b>	
11.57	4	536.23	2.7123	1.356	0.633	
8.83	8	623.35	2.7153	1.344	0.634	

TABLE II

Since the deviation in  $\kappa$  is not large it appears that the same type of relation holds so that one may write  $N_{G_{cr}}^2 = N_{G_{cr}|_{Ra}}^2 - \kappa Ra$ .

The difference in the first value of c is probably due to the absence of Prandtl Number effects. The eigenfunctions obtained are plotted in Fig. (5) together with the eigenfunctions of the second modal instability with Pr = 1. The neutral stability curves for  $R_n = 5$  and 10 and Pr = 1 are plotted in Fig. (6). They are, of course, scaled with the critical value of c . Figure (7) contains curves of the variation of critical Goertler Number with Rayleigh Number at the point of first instability.

The results evaluated for cases (d) and (e) are displayed in Figs. (8) and (9). The eigenfunctions drawn in Fig. (8) indicate the passage of the peak of the perturbations into the stable layer. The high value of the penetration coefficient and the extremely low value of the critical Rayleigh Number serve as reminders of the strongly unstable nature of the nonlinear thermal profiles. Therefore, it may be easily appreciated that such nonlinear profiles in the atmosphere (caused perhaps by latent heat release) could give rise to strongly penetrative disturbances resulting in considerable enhancement of the vertical transport of heat, momentum and moisture.

#### V. Conclusions

The object of this analysis was to explore the stability of parallel layers of fluid under the simultaneous influence of curvature and heating. The simple linear theory indicates not surprisingly, that the two effects are additive, demonstrating the close analogy between streamline curvature and buoyancy. A similar result has been obtained for the case of Thermohaline Convection by Lindberg (21) who arrives at the conclusion that the thermal Rayleigh Number and an analogously defined "Concentration Rayleigh Number" add linearly to form a stability parameter. The stability of a few nonlinear temperature profiles was investigated and their strongly penetrative nature demonstrated. Since such profiles are not uncommon in the atmosphere, it is reasonable to expect that convective instabilities could be generated in the lower layers, causing considerable modification of the vertical transport of heat, moisture and momentum, as is stated by Estoque (13).

Future work should include the interaction of the Tollmein Schlichting wave instabilities with truly three dimensional convective disturbances. The disturbances analyzed here have been quasi-twodimensional in that no variations in the streamwise direction have been assumed. The behavior of penetrative instabilities in an Ekman layer flow should also prove interesting since this approximates more closely the true atmospheric situation. Finally, the need for some simple nonlinear analyses to establish the interaction mechanism between the disturbances and the mean flow is now becoming of vital necessity.

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a - A Family of Parallel Curves



b - Dimensional Relationships





Figure 2. Perturbation Components for Case (a) Prandtl Number = 1













Figure 8. Temperature and Vertical Velocity Perturbations obtained for Cases (d) and (e)



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allows for the fact that in the atmosphere	e, convectio	n arising	in an unstable layer
may penetrate into a neignboring stable re	egion. ine	objective	has been to examine
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has been demonstrated. It is found that	for maralle!	lavers of	fluid along curved
heated walls, a unique stability curve for	r neutral di	sturbances	may be obtained if
the quantity plotted along the abscissa is	s Ra + $\kappa N_{G}^{2}$	where Ra	is the Rayleigh
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